# Hydroconversion of platform molecules of lignocellulosic origin into renewable fuel components

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Interreg, SKHU/1902/4.1/001/Bioeconomy

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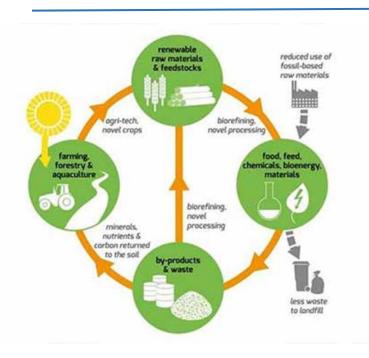








## Biomass conversion



Replacing fossil carbon by renewable alternatives

- Depleting resources
- Harmful effect on the environment
- Not carbon neutral, contribute to global warming

Conversion of waste biomass (non-edible and waste vegetable oils and animal fats) to biofuel or other valuable chemicals

• Carbon neutral: plants capture CO<sub>2</sub> through photosynthesis

## Biomass conversion to biofuels and other chemicals



Ethanol γ-Valerolactone (GVL)





Triglycerides (Tricaprylin)

Heterogeneous catalytic conversion



## I. Conversion of bioethanol into biobutanol

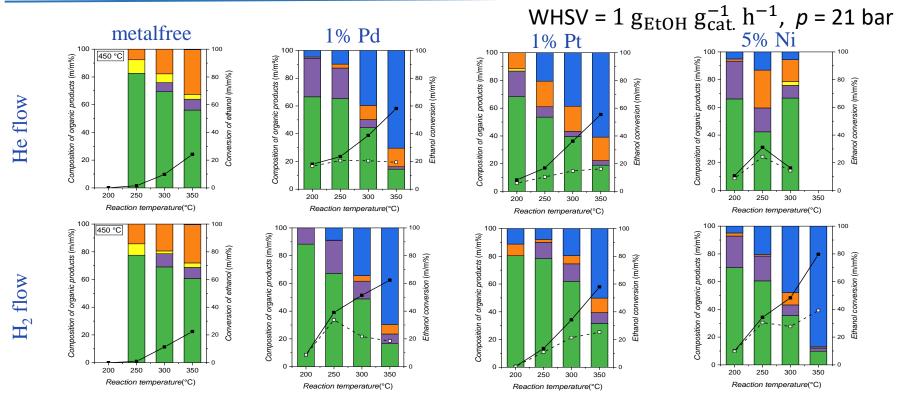
### Guerbet coupling reaction

#### Butanol formation via aldol condensation reaction

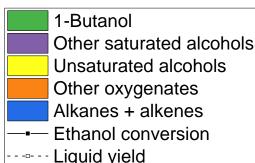
#### Butanol formation by chain mechanism

- Guerbet coupling of bioethanol produces biobutanol, which is an optional blending component of gasoline
- The catalyst must contain optimal balance of different catalytic functions: dehydrogenation/ hydrogenation, aldol addition, and dehydration.
- MgO-Al<sub>2</sub>O<sub>3</sub> mixed oxide catalyst modified with Pd, Pt, and Ni promoter.

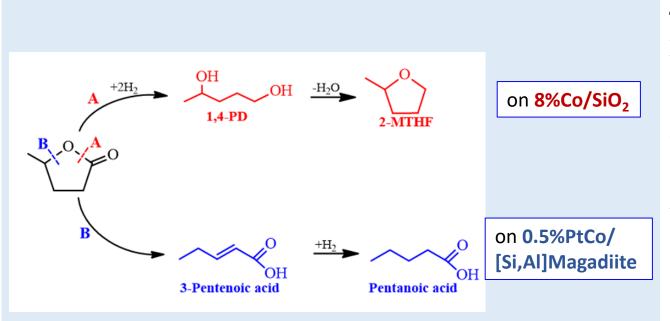
## I. Ethanol conversion on MgO-Al<sub>2</sub>O<sub>3</sub> catalysts



- Introduction of **metal modifiers** significantly improved the activity, whereas the alcohol yields decreased in the high temperature range.
- The selectivity loss is smaller in H<sub>2</sub> flow than in He flow over the Pd- and Pt-containing catalysts.
- At the lowest reaction temperature (200 °C) hydrogen hinders the initial dehydrogenation step of ethanol to acetaldehyde.



## II. Conversion of $\gamma$ -valerolactone to 2-methyltetrahydrofuran



Catalyst	Reaction temp., °C	Conversion, mol %	Selectivity, mol %				
			2-MTHF <sup>b</sup>	1,4-PD °	PA d	Pentanols <sup>e</sup>	Others
Co/SiO <sub>2</sub>	200 250	41.2 99.0	69.5 52.9	6.0 0	0	19.6 27.5	4.9 <sup>f</sup> 19.6 <sup>f</sup>
Pt/H-MAG	250 300	43.5 90.2	0.4 0	0 0	91.7 79.4	0.3 0.5	7.6 <sup>g</sup> 20.1 <sup>g</sup>

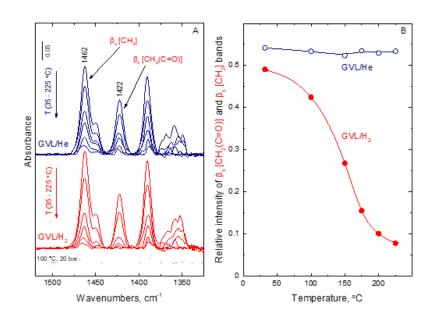
**γ-Valerolactone (GVL)** is produced in large amount from cellulosic biomass

**2-Methyltetrahydrofuran** is a valuable solvent in chemical industry and can be an additive to gasoline.

**Co/SiO<sub>2</sub>** (contains Lewis acid sites): catalyzes mainly reaction route "A"

**Pt/H-MAG** (contains both Lewis and Brönsted acid sites): catalyzes mainly reaction route "B"

# II. Operando DRIFT spectroscopy of GVL hydrogenation on Co/SiO<sub>2</sub> catalyst



$$\begin{array}{c|c} A \\ & & \\ \hline \\ GVL \\ & & \\ \hline \\ & & \\ \hline \\ & & \\ \hline \\ & & \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & & \\ \\ & & \\ \hline \\ & &$$

$$\delta_{as}[CH_3], \delta_s[CH_3]$$

$$0$$

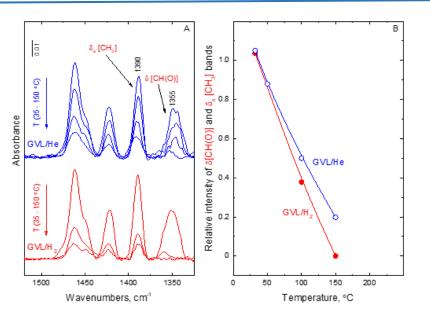
$$\delta[CH(O)]$$

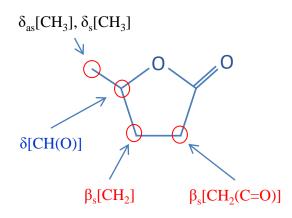
$$\beta_s[CH_2]$$

$$\beta_s[CH_2(C=O)]$$

- -In contact with GVL/He flow: only the adsorption coverage of the catalyst changes.
- -In contact with GVL/H<sub>2</sub> flow: GVL transformation takes place.
- -Hydrogenation reaction eliminates the carbonyl group, whereas the 5-member ring is not affected.

## II. Operando DRIFT spectroscopy of GVL hydrogenation on Pt/H-MAG catalyst





- -Regardless of the applied carrier gas (GVL/He or GVL/H<sub>2</sub> flow) GVL transformation takes place.
- -Results suggest that the cleavage of the C-O bond in the GVL ring occurs on the methyl side. The most probable reaction intermediate is pentenoic acid.

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## III. Conversion of triglycerides to diesel fuels

#### First step: hydrogenolysis of the ester bonds

#### Converversion of carboxylic acid, not fully understood

1. hydrodecarbonylation: formation of CO

$$R \xrightarrow{O} OH \xrightarrow{H_2} [R-CH_3 \cdots HCOOH] \longrightarrow R-CH_3 + CO + H_2O$$

2. hydrodecarboxylation: formation of CO<sub>2</sub>

$$R \leftarrow CH_2 \rightarrow CH_3 + CO_2$$

2. H<sub>2</sub>-reduction of oxygen: formation of H<sub>2</sub>O via consecutive hydrogen addition and dehydration steps

$$R \xrightarrow{O} OH \xrightarrow{3 \text{ H}_2} R-CH_2-CH_3 + 2 \text{ H}_2O$$

#### **Catalytic hydrodeoxygenation**

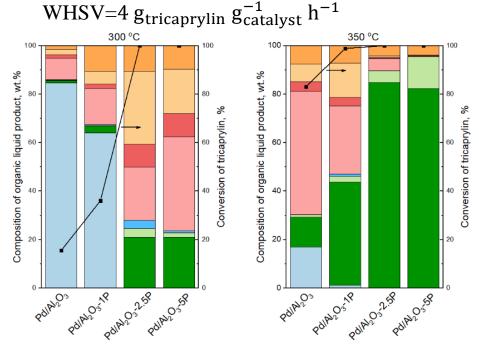
(HDO) of bio-oils is more advantageous than the transesterification with ethanol or methanol.

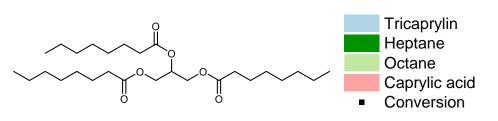
The product **bio-gasoil** mainly contains C15–C18 alkanes.

Can be used as an alternative diesel fuel without the modification of internal combustion engines.

# III. HDO reaction of tricaprylin on phosphatized Al<sub>2</sub>O<sub>3</sub>-supported Pd catalysts

Model triglceride: tricapryline 20 bar, in H<sub>2</sub> flow,





- Pd/Al<sub>2</sub>O<sub>3</sub> catalysts show high activity in hydrogenolysis of the ester bonds (1<sup>st</sup> step).
- Yield of paraffin products (heptane and octane) dramatically increased with the phosphorous content (nearly 100 % on Pd/Al<sub>2</sub>O<sub>3</sub>-5P).



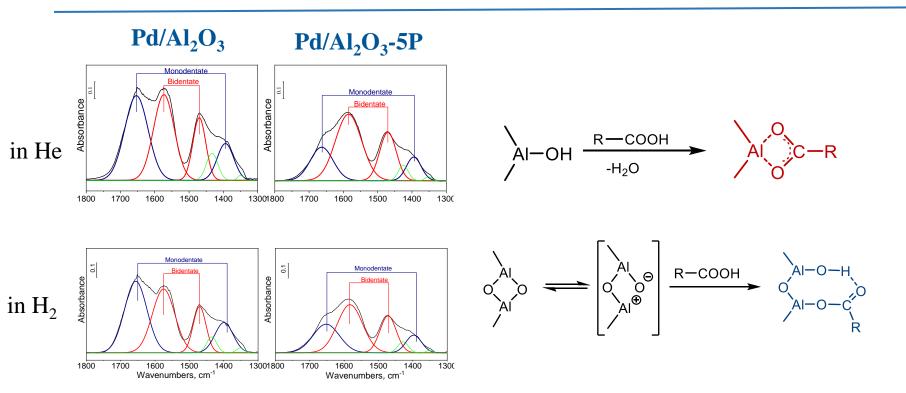
- Change of catalyst structure
- o Enhanced HDO (mainly

hydrodecarbonylation) activity

$$R \xrightarrow{O \ CH_2 \ OH} \xrightarrow{H_2} R-CH_3 + CO + H_2O$$

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# III. Operando DRIFT spectroscopy of valeric acid hydroconversion



- Phosphatization significantly decrease the concentration of **monodentate** species.
- Bidentate carboxylate species are more reactive with H<sub>2</sub> than the monodentate species.

$$AI$$
  $C-R$   $\xrightarrow{2H}$   $AI$   $+$   $HC-R$ 

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## **Summary**

- The effect of metal modifiers in Guerbet coupling of bioethanol to butanol was investigated on mixed Mg-Al oxide based catalysts.
  - Gasoline additive biobutanol was produced in high yields on Pd and Pt modified catalysts.
- Hydrogenation of GVL over 8%Co/SiO2 catalyst shows high selectivity towards 2-MTHF, whereas 0.5%Pt/H-Magadiite catalyst catalyzed the GVL conversion to pentanoic acid with >90% selectivity.
  - The results of the operando DRIFT spectroscopic investigations allowed us to propose a plausible reaction mechanism over both bifuntional catalyst.
- Surface phosphatization of the  $\gamma$ -alumina support significantly increased the HDO activity of the Pd catalyst to convert tricapryline into paraffinic hydrocarbons (bio-gasoil). The operando DRIFT measurements revealed the origin of the increased HDO activity.

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## Thank you for your kind attention!

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**Building Partnership**